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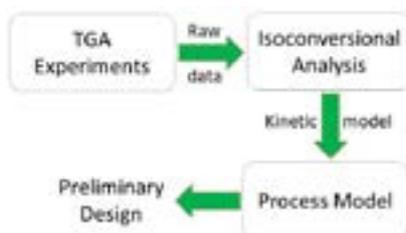
13th Global Summit and Expo on Biomass and Bioenergy

September 04-06, 2018 | Zurich, Switzerland

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Biomass thermochemical processes suffer from the problem of feedstock variation. In the other words, in order to run commercial biomass-based plants under economically feasible conditions, the process have to be capable of handling very different raw materials, ranging from forest residues to waste materials from various industries. Process modeling is crucial to predict the behavior of different feedstock materials in a given biomass plant. In this work, we consider the slow pyrolysis of biomass to produce biochar. In this process, the main quantity one aims at predicting by means of process modelling is the conversion of raw biomass to biochar as a function of the process conditions. To achieve this aim, the process model requires a kinetic rate expression for describing the evolution of the biomass when subject to thermochemical treatment. Here, we will show that the TGA data processed with an isoconversional method is enough to obtain an effective rate expression which allows for predicting the behavior of the biomass at an arbitrary temperature evolution. Such rate expressions can then be used in the process model to simulate conversion of raw biomass to biochar. An overview of this approach is shown in Figure 1. To illustrate the feasibility of the approach we will consider different biomasses feedstocks undergoing slow pyrolysis in an indirectly heated rotary kiln reactor. The results of our modeling are then compared to experimental data obtained from a 500 kW pilot plant pyrolyzer and to a more detailed process model. A high level of agreement between the modeling results from this approach and the experimental data and the previously validate detailed process model is observed. This proves the capability of our cost-efficient approach to obtain preliminary design data.



Recent Publications

1. Sadegh-Vaziri, R., Amovic, M., Ljunggren, R., & Engvall, K. (2015). A Medium-Scale 50 MW fuel Biomass Gasification Based Bio-SNG Plant: A Developed Gas Cleaning Process. *Energies*, 8(6), 5287-5302.
2. Sadegh-Vaziri, R., & Babler, M. U. (2017). Numerical investigation of the outward growth of ZnS in the removal of H₂S in a packed bed of ZnO. *Chemical Engineering Science*, 158, 328-339.
3. Sadegh-Vaziri, R., & Babler, M. U. (2017). PBE Modeling of Flocculation of Microalgae: Investigating the Overshoot in Mean Size Profiles. *Energy Procedia*, 142, 507-512.
4. Babler, M. U., Phounglamcheik, A., Amovic, M., Ljunggren, R., & Engvall, K. (2017). Modeling and pilot plant runs of slow biomass pyrolysis in a rotary kiln. *Applied Energy*, 207, 123-133.
5. Samuelsson, L. N., Umeki, K., & Babler, M. U. (2017). Mass loss rates for wood chips at isothermal pyrolysis conditions: A comparison with low heating rate powder data. *Fuel Processing Technology*, 158, 26-34.

Biography

5DPLDU 6DGHJK 9DJLUL LV D 3K' FDQGLGDWH DW WKH GHSDUWPHQW RI FKHPDFDO HQJLQHHULQJ DW .7+ URV PRGHOLQJ DQG QXPULFDO VLPXODWLRQ +H KDV ZRUNHG RQ GLIIHUHQW SURMHFWV LQFOXGLQJ UDZ V\Q WXUEXOHQW ARZV ELRPDVV S\URO\VLV DQG JDLV\FDWLRQ DQG PRGHOLQJ RI VXSSRUWHG OLTXLG PHPEUD KLV NQRZOHGJH RI &)' PRGHOLQJ DQG QXPULFDO GLVFUHWLJDWLRQ RI SDUWLDO GLIIHUHQWLDO DQG LQWH

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